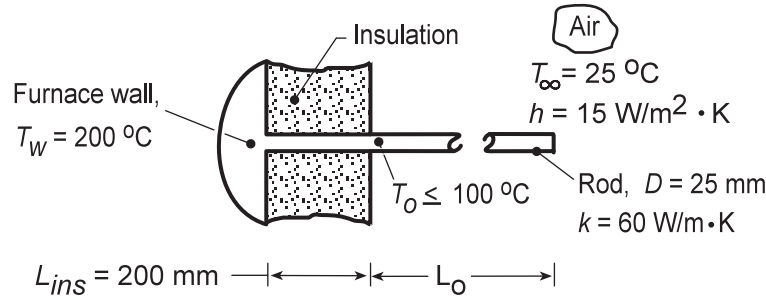


### PROBLEM 3.122

**KNOWN:** Rod protruding normally from a furnace wall covered with insulation of thickness  $L_{ins}$  with the length  $L_o$  exposed to convection with ambient air.

**FIND:** (a) An expression for the exposed surface temperature  $T_o$  as a function of the prescribed thermal and geometrical parameters. (b) Will a rod of  $L_o = 100$  mm meet the specified operating limit,  $T_o \leq 100^\circ\text{C}$ ? If not, what design parameters would you change?

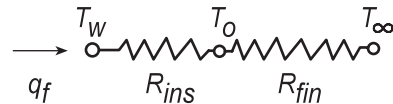
**SCHEMATIC:**



**ASSUMPTIONS:** (1) Steady-state conditions, (2) One-dimensional conduction in rod, (3) Negligible thermal contact resistance between the rod and hot furnace wall, (4) Insulated section of rod,  $L_{ins}$ , experiences no lateral heat losses, (5) Convection coefficient uniform over the exposed portion of the rod,  $L_o$ , (6) Adiabatic tip condition for the rod and (7) Negligible radiation exchange between rod and its surroundings.

**ANALYSIS:** (a) The rod can be modeled as a thermal network comprised of two resistances in series: the portion of the rod,  $L_{ins}$ , covered by insulation,  $R_{ins}$ , and the portion of the rod,  $L_o$ , experiencing convection, and behaving as a fin with an adiabatic tip condition,  $R_{fin}$ . For the insulated section:

$$R_{ins} = L_{ins} / kA_c \quad (1)$$



For the fin, Table 3.4, Case B, Eq. 3.81,

$$R_{fin} = \theta_b / q_f = \frac{1}{(hPkA_c)^{1/2} \tanh(mL_o)} \quad (2)$$

$$m = (hP/kA_c)^{1/2} \quad A_c = \pi D^2 / 4 \quad P = \pi D \quad (3,4,5)$$

From the thermal network, by inspection,

$$\frac{T_o - T_\infty}{R_{fin}} = \frac{T_W - T_\infty}{R_{ins} + R_{fin}} \quad T_o = T_\infty + \frac{R_{fin}}{R_{ins} + R_{fin}} (T_W - T_\infty) \quad (6) <$$

(b) Substituting numerical values into Eqs. (1) - (6) with  $L_o = 200$  mm,

$$T_o = 25^\circ\text{C} + \frac{6.298}{6.790 + 6.298} (200 - 25)^\circ\text{C} = 109^\circ\text{C} <$$

$$R_{ins} = \frac{0.200 \text{ m}}{60 \text{ W/m} \cdot \text{K} \times 4.909 \times 10^{-4} \text{ m}^2} = 6.790 \text{ K/W} \quad A_c = \pi (0.025 \text{ m})^2 / 4 = 4.909 \times 10^{-4} \text{ m}^2$$

$$R_{fin} = 1 / \left( (0.0347 \text{ W}^2 / \text{K}^2) \right)^{1/2} \tanh(6.324 \times 0.200) = 6.298 \text{ K/W}$$

$$(hPkA_c) = \left( 15 \text{ W/m}^2 \cdot \text{K} \times \pi (0.025 \text{ m}) \times 60 \text{ W/m} \cdot \text{K} \times 4.909 \times 10^{-4} \text{ m}^2 \right) = 0.0347 \text{ W}^2 / \text{K}^2$$

Continued...

### PROBLEM 3.122 (Cont.)

$$m = (hP/kA_c)^{1/2} = \left(15 \text{ W/m}^2 \cdot \text{K} \times \pi (0.025 \text{ m}) / 60 \text{ W/m} \cdot \text{K} \times 4.909 \times 10^{-4} \text{ m}^2\right)^{1/2} = 6.324 \text{ m}^{-1}$$

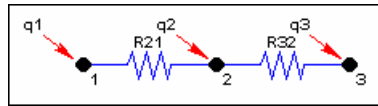
Consider the following design changes aimed at reducing  $T_o \leq 100^\circ\text{C}$ . (1) Increasing length of the fin portions: with  $L_o = 400$  and  $600$  mm,  $T_o$  is  $102.8^\circ\text{C}$  and  $102.3^\circ\text{C}$ , respectively. Hence, increasing  $L_o$  will reduce  $T_o$  only modestly. (2) Decreasing the thermal conductivity: backsolving the above equation set with  $T_o = 100^\circ\text{C}$ , find the required thermal conductivity is  $k = 14 \text{ W/m}\cdot\text{K}$ . Hence, we could select a stainless steel alloy; see Table A.1. (3) Increasing the insulation thickness: find that for  $T_o = 100^\circ\text{C}$ , the required insulation thickness would be  $L_{\text{ins}} = 211 \text{ mm}$ . This design solution might be physically and economically unattractive. (4) A very practical solution would be to introduce thermal contact resistance between the rod base and the furnace wall by “tack welding” (rather than a continuous bead around the rod circumference) the rod in two or three places. (5) A less practical solution would be to increase the convection coefficient, since to do so, would require an air handling unit. (6) Using a tube rather than a rod will decrease  $A_c$ . For a 3 mm tube wall and 25 mm outside diameter,  $A_c = 2.07 \times 10^{-4} \text{ m}^2$ ,  $R_{\text{ins}} = 16.103 \text{ K/W}$  and  $R_{\text{fin}} = 8.61 \text{ K/W}$ , yielding  $T_o = 86^\circ\text{C}$ . (conduction within the air inside the tube is neglected).

**COMMENTS:** (1) Would replacing the rod by a thick-walled tube provide a practical solution?

(2) The *IHT Thermal Resistance Network Model* and the *Thermal Resistance Tool* for a fin with an *adiabatic tip* were used to create a model of the rod. The Workspace is shown below.

// Thermal Resistance Network Model:

// The Network:



// Heat rates into node j,qij, through thermal resistance Rij

$$q_{21} = (T_2 - T_1) / R_{21}$$

$$q_{32} = (T_3 - T_2) / R_{32}$$

// Nodal energy balances

$$q_1 + q_{21} = 0$$

$$q_2 - q_{21} + q_{32} = 0$$

$$q_3 - q_{32} = 0$$

/\* Assigned variables list: deselect the qi, Rij and Ti which are unknowns; set qi = 0 for embedded nodal points at which there is no external source of heat. \*/

T1 = Tw // Furnace wall temperature, C

//q1 = // Heat rate, W

T2 = To // To, beginning of rod exposed length

q2 = 0 // Heat rate, W; node 2; no external heat source

T3 = Tinf // Ambient air temperature, C

//q3 = // Heat rate, W

**// Thermal Resistances:**

// Rod - conduction resistance

$$R_{21} = L_{\text{ins}} / (k * A_c) // \text{Conduction resistance, K/W}$$

$$A_c = \pi * D^2 / 4 // \text{Cross sectional area of rod, m}^2$$

**// Thermal Resistance Tools - Fin with Adiabatic Tip:**

$$R_{32} = R_{\text{fin}} // \text{Resistance of fin, K/W}$$

/\* Thermal resistance of a fin of uniform cross sectional area  $A_c$ , perimeter  $P$ , length  $L$ , and thermal conductivity  $k$  with an adiabatic tip condition experiencing convection with a fluid at  $T_{\text{inf}}$  and coefficient  $h$ , \*/

$$R_{\text{fin}} = 1 / ( \tanh(m * L_o) * (h * P * k * A_c)^{1/2} ) // \text{Case B, Table 3.4}$$

$$m = \sqrt{h * P / (k * A_c)}$$

$$P = \pi * D // \text{Perimeter, m}$$

**// Other Assigned Variables:**

Tw = 200 // Furnace wall temperature, C

k = 60 // Rod thermal conductivity, W/m.K

Lins = 0.200 // Insulated length, m

D = 0.025 // Rod diameter, m

h = 15 // Convection coefficient, W/m^2.K

Tinf = 25 // Ambient air temperature, C

Lo = 0.200 // Exposed length, m