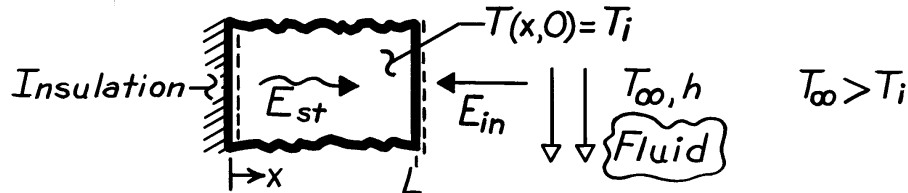


PROBLEM 2.57

KNOWN: Plane wall, initially at a uniform temperature, is suddenly exposed to convective heating.

FIND: (a) Differential equation and initial and boundary conditions which may be used to find the temperature distribution, $T(x,t)$; (b) Sketch $T(x,t)$ for these conditions: initial ($t \leq 0$), steady-state, $t \rightarrow \infty$, and two intermediate times; (c) Sketch heat fluxes as a function of time for surface locations; (d) Expression for total energy transferred to wall per unit volume (J/m^3).

SCHEMATIC:



ASSUMPTIONS: (1) One-dimensional conduction, (2) Constant properties, (3) No internal heat generation.

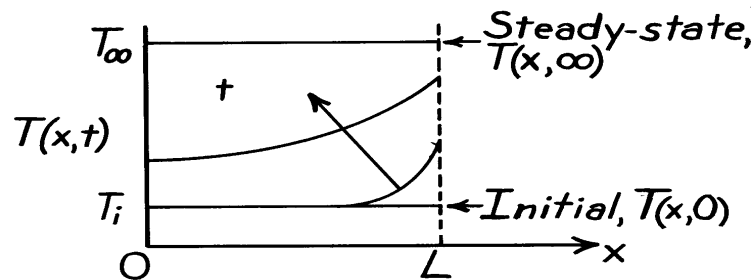
ANALYSIS: (a) For one-dimensional conduction with constant properties, the heat equation has the form,

$$\frac{\partial^2 T}{\partial x^2} = \frac{1}{\alpha} \frac{\partial T}{\partial t}$$

and the conditions are:

$$\begin{cases} \text{Initial, } t \leq 0: & T(x,0) = T_i \\ \text{Boundaries: } & x=0 \quad \frac{\partial T}{\partial x}\bigg|_0 = 0 \\ & x=L \quad -k \frac{\partial T}{\partial x}\bigg|_L = h[T(L,t) - T_\infty] \end{cases} \quad \begin{array}{l} \text{uniform} \\ \text{adiabatic} \\ \text{convection} \end{array}$$

(b) The temperature distributions are shown on the sketch.

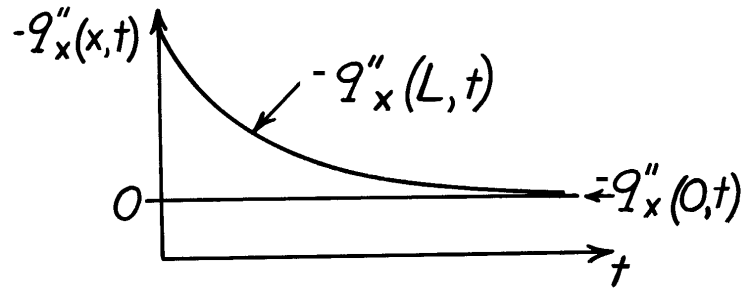


Note that the gradient at $x = 0$ is always zero, since this boundary is adiabatic. Note also that the gradient at $x = L$ decreases with time.

(c) The heat flux, $q_x''(x,t)$, as a function of time, is shown on the sketch for the surfaces $x = 0$ and $x = L$.

Continued ...

PROBLEM 2.57 (Cont.)



For the surface at $x = 0$, $q''_x(0, t) = 0$ since it is adiabatic. At $x = L$ and $t = 0$, $q''_x(L, 0)$ is a maximum (in magnitude)

$$|q''_x(L, 0)| = h |T(L, 0) - T_\infty|$$

where $T(L, 0) = T_i$. The temperature difference, and hence the flux, decreases with time.

(d) The total energy transferred to the wall may be expressed as

$$E_{\text{in}} = \int_0^\infty q''_{\text{conv}} A_s dt$$

$$E_{\text{in}} = h A_s \int_0^\infty (T_\infty - T(L, t)) dt$$

Dividing both sides by $A_s L$, the energy transferred per unit volume is

$$\frac{E_{\text{in}}}{V} = \frac{h}{L} \int_0^\infty [T_\infty - T(L, t)] dt \quad \left[\text{J/m}^3 \right]$$

COMMENTS: Note that the heat flux at $x = L$ is into the wall and is hence in the negative x direction.