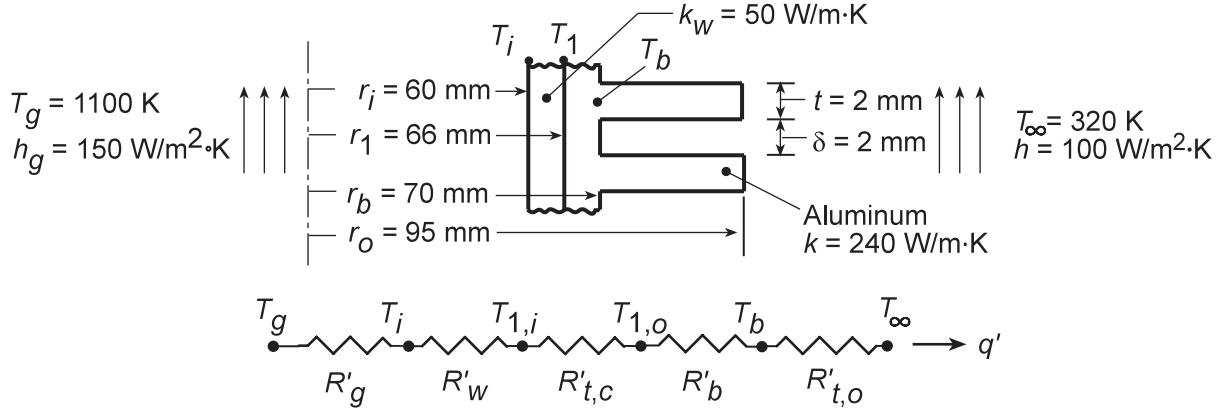


### PROBLEM 3.161

**KNOWN:** Dimensions and materials of a finned (annular) cylinder wall. Combustion gas and ambient air conditions. Contact resistance.

**FIND:** (a) Heat rate per unit length and surface and interface temperatures, (b) Effect of increasing the fin thickness.

**SCHEMATIC:**



**ASSUMPTIONS:** (1) One-dimensional, steady-state conditions, (2) Constant properties, (3) Uniform  $h$  over surfaces, (4) Negligible radiation.

**ANALYSIS:** (a) The heat rate per unit length is

$$q' = \frac{T_g - T_\infty}{R'_{\text{tot}}}$$

where  $R'_{\text{tot}} = R'_g + R'_w + R'_{t,c} + R'_b + R'_{t,o}$ , and

$$R'_g = (h_g 2\pi r_i)^{-1} = (150 \text{ W/m}^2 \cdot \text{K} \times 2\pi \times 0.06 \text{ m})^{-1} = 0.0177 \text{ m} \cdot \text{K/W},$$

$$R'_w = \frac{\ln(r_1/r_i)}{2\pi k_w} = \frac{\ln(66/60)}{2\pi (50 \text{ W/m} \cdot \text{K})} = 3.03 \times 10^{-4} \text{ m} \cdot \text{K/W},$$

$$R'_{t,c} = (R'_{t,c}/2\pi r_1) = 10^{-4} \text{ m}^2 \cdot \text{K/W} / 2\pi \times 0.066 \text{ m} = 2.41 \times 10^{-4} \text{ m} \cdot \text{K/W}$$

$$R'_b = \frac{\ln(r_b/r_1)}{2\pi k} = \frac{\ln(70/66)}{2\pi \times 240 \text{ W/m} \cdot \text{K}} = 3.90 \times 10^{-5} \text{ m} \cdot \text{K/W},$$

$$R'_{t,o} = (\eta_o h A'_t)^{-1},$$

$$\eta_o = 1 - \frac{N' A_f}{A'_t} (1 - \eta_f),$$

$$A_f = 2\pi (r_{oc}^2 - r_b^2)$$

$$A'_t = N' A_f + (1 - N' t) 2\pi r_b$$

$$\eta_f = \frac{(2r_b/m) K_1(mr_b) I_1(mr_{oc}) - I_1(mr_b) K_1(mr_{oc})}{(r_{oc}^2 - r_b^2) I_0(mr_1) K_1(mr_{oc}) + K_0(mr_b) I_1(mr_{oc})}$$

$$r_{oc} = r_o + (t/2), \quad m = (2h/kt)^{1/2}$$

Continued...

### PROBLEM 3.161 (Cont.)

Once the heat rate is determined from the foregoing expressions, the desired interface temperatures may be obtained from

$$T_i = T_g - q'R'_g$$

$$T_{l,i} = T_g - q'(R'_g + R'_w)$$

$$T_{l,o} = T_g - q'(R'_g + R'_w + R'_{t,c})$$

$$T_b = T_g - q'(R'_g + R'_w + R'_{t,c} + R'_b)$$

For the specified conditions we obtain  $A'_t = 7.00 \text{ m}$ ,  $\eta_f = 0.902$ ,  $\eta_o = 0.906$  and  $R'_{t,o} = 0.00158 \text{ m}\cdot\text{K}/\text{W}$ . It follows that

$$q' = 39,300 \text{ W/m} \quad <$$

$$T_i = 405\text{K}, \quad T_{l,i} = 393\text{K}, \quad T_{l,o} = 384\text{K}, \quad T_b = 382\text{K} \quad <$$

(b) The *Performance Calculation, Extended Surface* Model for the *Circular Fin* Array may be used to assess the effects of fin thickness and spacing. Increasing the fin thickness to  $t = 3 \text{ mm}$ , with  $\delta = 2 \text{ mm}$ , reduces the number of fins per unit length to 200. Hence, although the fin efficiency increases ( $\eta_f = 0.930$ ), the reduction in the total surface area ( $A'_t = 5.72 \text{ m}$ ) yields an increase in the resistance of the fin array ( $R'_{t,o} = 0.00188 \text{ m}\cdot\text{K}/\text{W}$ ), and hence a reduction in the heat rate ( $q' = 38,700 \text{ W/m}$ ) and an increase in the interface temperatures ( $T_i = 415 \text{ K}$ ,  $T_{l,i} = 404 \text{ K}$ ,  $T_{l,o} = 394 \text{ K}$ , and  $T_b = 393 \text{ K}$ ).

**COMMENTS:** Because the gas convection resistance exceeds all other resistances by at least an order of magnitude, incremental changes in  $R'_{t,o}$  will not have a significant effect on  $q'$  or the interface temperatures.