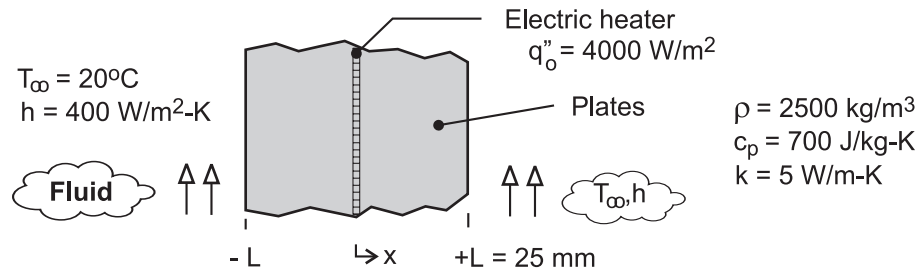


## PROBLEM 2.53

**KNOWN:** Thin electrical heater dissipating  $4000 \text{ W/m}^2$  sandwiched between two 25-mm thick plates whose surfaces experience convection.

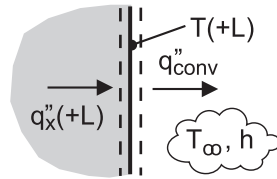
**FIND:** (a) On T-x coordinates, sketch the steady-state temperature distribution for  $-L \leq x \leq +L$ ; calculate values for the surfaces  $x = \pm L$  and the mid-point,  $x = 0$ ; label this distribution as Case 1 and explain key features; (b) Case 2: sudden loss of coolant causing existence of adiabatic condition on the  $x = +L$  surface; sketch temperature distribution on same T-x coordinates as part (a) and calculate values for  $x = 0, \pm L$ ; explain key features; (c) Case 3: further loss of coolant and existence of adiabatic condition on the  $x = -L$  surface; situation goes undetected for 15 minutes at which time power to the heater is deactivated; determine the eventual ( $t \rightarrow \infty$ ) uniform, steady-state temperature distribution; sketch temperature distribution on same T-x coordinates as parts (a,b); and (d) On T-t coordinates, sketch the temperature-time history at the plate locations  $x = 0, \pm L$  during the transient period between the steady-state distributions for Case 2 and Case 3; at what location and when will the temperature in the system achieve a maximum value?

**SCHEMATIC:**



**ASSUMPTIONS:** (1) One-dimensional conduction, (2) Constant properties, (3) No internal volumetric generation in plates, and (3) Negligible thermal resistance between the heater surfaces and the plates.

**ANALYSIS:** (a) Since the system is symmetrical, the heater power results in equal conduction fluxes through the plates. By applying a surface energy balance on the surface  $x = +L$  as shown in the schematic, determine the temperatures at the mid-point,  $x = 0$ , and the exposed surface,  $x = +L$ .



$$\dot{E}_{\text{in}} - \dot{E}_{\text{out}} = 0$$

$$q''_x(+L) - q''_{\text{conv}} = 0 \quad \text{where} \quad q''_x(+L) = q''_0 / 2$$

$$q''_0 / 2 - h[T(+L) - T_\infty] = 0$$

$$T_1(+L) = q''_0 / 2h + T_\infty = 4000 \text{ W/m}^2 / (2 \times 400 \text{ W/m}^2 \cdot \text{K}) + 20^\circ\text{C} = 25^\circ\text{C} \quad <$$

From Fourier's law for the conduction flux through the plate, find  $T(0)$ .

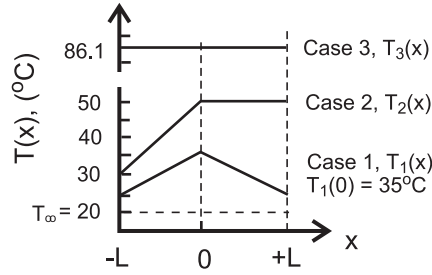
$$q''_x = q''_0 / 2 = k[T(0) - T(+L)] / L$$

$$T_1(0) = T_1(+L) + q''_0 L / 2k = 25^\circ\text{C} + 4000 \text{ W/m}^2 \cdot \text{K} \times 0.025 \text{ m} / (2 \times 5 \text{ W/m} \cdot \text{K}) = 35^\circ\text{C} \quad <$$

The temperature distribution is shown on the T-x coordinates below and labeled Case 1. The key features of the distribution are its symmetry about the heater plane and its linear dependence with distance.

Continued ...

### PROBLEM 2.53 (Cont.)



(b) Case 2: sudden loss of coolant with the existence of an adiabatic condition on surface  $x = +L$ . For this situation, all the heater power will be conducted to the coolant through the left-hand plate. From a surface energy balance and application of Fourier's law as done for part (a), find

$$T_2(-L) = q_0'' / h + T_\infty = 4000 \text{ W/m}^2 / 400 \text{ W/m}^2 \cdot \text{K} + 20^\circ\text{C} = 30^\circ\text{C} \quad <$$

$$T_2(0) = T_2(-L) + q_0'' L / k = 30^\circ\text{C} + 4000 \text{ W/m}^2 \times 0.025 \text{ m} / 5 \text{ W/m} \cdot \text{K} = 50^\circ\text{C} \quad <$$

The temperature distribution is shown on the  $T$ - $x$  coordinates above and labeled Case 2. The distribution is linear in the left-hand plate, with the maximum value at the mid-point. Since no heat flows through the right-hand plate, the gradient must be zero and this plate is at the maximum temperature as well. The maximum temperature is higher than for Case 1 because the heat flux through the left-hand plate has increased two-fold.

(c) Case 3: sudden loss of coolant occurs at the  $x = -L$  surface also. For this situation, there is no heat transfer out of either plate, so that for a 15-minute period,  $\Delta t_0$ , the heater dissipates  $4000 \text{ W/m}^2$  and then is deactivated. To determine the eventual, uniform steady-state temperature distribution, apply the conservation of energy requirement on a time-interval basis, Eq. 1.12b. The initial condition corresponds to the temperature distribution of Case 2, and the final condition will be a uniform, elevated temperature  $T_f = T_3$  representing Case 3. We have used  $T_\infty$  as the reference condition for the energy terms.

$$E_{\text{in}}'' - E_{\text{out}}'' + E_{\text{gen}}'' = \Delta E_{\text{st}}'' = E_f'' - E_i'' \quad (1)$$

Note that  $E_{\text{in}}'' - E_{\text{out}}'' = 0$ , and the dissipated electrical energy is

$$E_{\text{gen}}'' = q_0'' \Delta t_0 = 4000 \text{ W/m}^2 (15 \times 60) \text{ s} = 3.600 \times 10^6 \text{ J/m}^2 \quad (2)$$

For the final condition,

$$\begin{aligned} E_f'' &= \rho c (2L) [T_f - T_\infty] = 2500 \text{ kg/m}^3 \times 700 \text{ J/kg} \cdot \text{K} (2 \times 0.025 \text{ m}) [T_f - 20]^\circ\text{C} \\ E_f'' &= 8.75 \times 10^4 [T_f - 20] \text{ J/m}^2 \end{aligned} \quad (3)$$

where  $T_f = T_3$ , the final uniform temperature, Case 3. For the initial condition,

$$E_i'' = \rho c \int_{-L}^{+L} [T_2(x) - T_\infty] dx = \rho c \left\{ \int_{-L}^0 [T_2(x) - T_\infty] dx + \int_0^{+L} [T_2(0) - T_\infty] dx \right\} \quad (4)$$

where  $T_2(x)$  is linear for  $-L \leq x \leq 0$  and constant at  $T_2(0)$  for  $0 \leq x \leq +L$ .

$$\begin{aligned} T_2(x) &= T_2(0) + [T_2(0) - T_2(L)] x / L & -L \leq x \leq 0 \\ T_2(x) &= 50^\circ\text{C} + [50 - 30]^\circ\text{C} x / 0.025 \text{ m} \\ T_2(x) &= 50^\circ\text{C} + 800x \end{aligned} \quad (5)$$

Substituting for  $T_2(x)$ , Eq. (5), into Eq. (4)

Continued ...

### PROBLEM 2.53 (Cont.)

$$\begin{aligned}
 E_1'' &= \rho c \left\{ \int_{-L}^0 [50 + 800x - T_\infty] dx + [T_2(0) - T_\infty] L \right\} \\
 E_1'' &= \rho c \left\{ \left[ 50x + 400x^2 - T_\infty x \right]_{-L}^0 + [T_2(0) - T_\infty] L \right\} \\
 E_1'' &= \rho c \left\{ -[-50L + 400L^2 + T_\infty L] + [T_2(0) - T_\infty] L \right\} \\
 E_1'' &= \rho c L \{ +50 - 400L - T_\infty + T_2(0) - T_\infty \} \\
 E_1'' &= 2500 \text{ kg/m}^3 \times 700 \text{ J/kg} \cdot \text{K} \times 0.025 \text{ m} \{ +50 - 400 \times 0.025 - 20 + 50 - 20 \} \text{ K} \\
 E_1'' &= 2.188 \times 10^6 \text{ J/m}^2 \quad (6)
 \end{aligned}$$

Returning to the energy balance, Eq. (1), and substituting Eqs. (2), (3) and (6), find  $T_f = T_3$ .

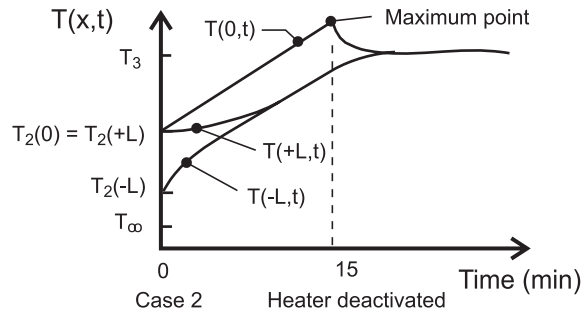
$$3.600 \times 10^6 \text{ J/m}^2 = 8.75 \times 10^4 [T_3 - 20] - 2.188 \times 10^6 \text{ J/m}^2$$

$$T_3 = (66.1 + 20)^\circ\text{C} = 86.1^\circ\text{C}$$

<

The temperature distribution is shown on the T-x coordinates above and labeled Case 3. The distribution is uniform, and considerably higher than the maximum value for Case 2.

(d) The temperature-time history at the plate locations  $x = 0, \pm L$  during the transient period between the distributions for Case 2 and Case 3 are shown on the T-t coordinates below.



Note the temperatures for the locations at time  $t = 0$  corresponding to the instant when the surface  $x = -L$  becomes adiabatic. These temperatures correspond to the distribution for Case 2. The heater remains energized for yet another 15 minutes and then is deactivated. The midpoint temperature,  $T(0,t)$ , is always the hottest location and the maximum value slightly exceeds the final temperature  $T_3$ .