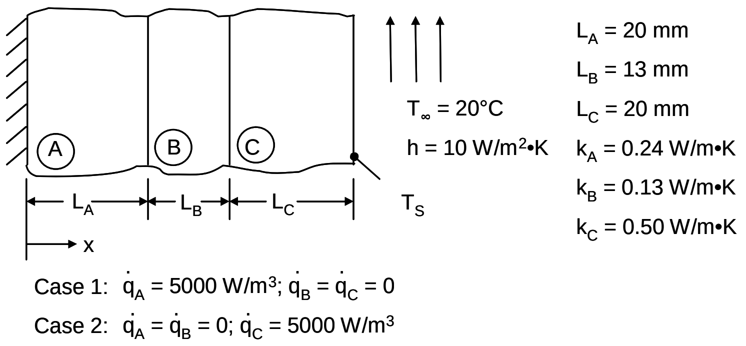
PROBLEM 3.85

KNOWN: Dimensions and properties of a composite wall exposed to convective or insulated conditions.

FIND: (a) Maximum wall temperature for left face insulated and right face convectively cooled, (b) Sketch the steady-state temperature distribution of part (a), (c) Sketch the steady-state temperature distribution with reversed boundary conditions.

SCHEMATIC:



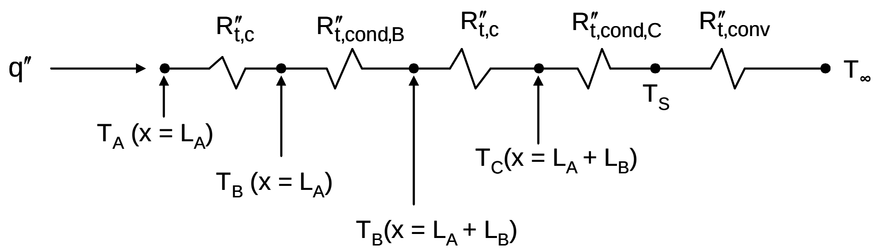
ASSUMPTIONS: (1) Steady-state conditions, (2) One-dimensional heat transfer, (3) Uniform volumetric energy generation.

ANALYSIS:

(a) The heat flux through materials B and C is constant and is

$$q'' = \dot{q}_A (L_A) = 5000\ W/m^3 \times 0.02\ m = 100\ W/m^2$$

The thermal resistance network that spans from $x = L_A$ to the coolant is



The thermal resistances are:

$$R''_{t,c} = 0.01 m^2 \cdot K/w$$

$$R''_{t,cond,B} = \frac{L_B}{k_B} = \frac{0.013\ m}{0.13\ W/m \cdot K} = 0.1\ \frac{m^2 \cdot K}{W}$$

$$R''_{t,cond,C} = \frac{L_C}{k_C} = \frac{0.020\ m}{0.50\ W/m \cdot K} = 0.04\ \frac{m^2 \cdot K}{W}$$

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$$R''_{t,conv} = \frac{1}{h} = \frac{1}{10\ \mathrm{W/m^2 \cdot K}} = 0.1\ \frac{\mathrm{m^2 \cdot K}}{\mathrm{W}}$$

The total thermal resistance is

$$R''_{t,tot} = (0.01 + 0.1 + 0.01 + 0.04 + 0.1) = 0.26\ \frac{\mathrm{m^2 \cdot K}}{\mathrm{W}}$$

Therefore,

$$T_A(x{=}L_A) = q''(R''_{t,tot}) + T_\infty = 100\ \mathrm{W/m^2} \times 0.26\ \frac{\mathrm{m^2 \cdot K}}{\mathrm{W}} + 20°\mathrm{C} = 46°\mathrm{C}$$

The maximum temperature occurs at x = 0 and may be evaluated by using Eq. 3.48 as follows

$$T_A(x{=}0) = T_A(x{=}L_A) + \frac{\dot{q}_A L_A^2}{2k_A} = 46°\mathrm{C} + \frac{5000\ \mathrm{W/m^3} \times (0.02\ \mathrm{m})^2}{2 \times 0.24\ \mathrm{W/m \cdot K}}$$

$T_A(x{=}0) = T_{max} = 50.2°\mathrm{C}$ <

(b) To sketch the temperature distribution, we begin by evaluating the temperatures shown in the thermal resistance network. Working from the coolant side,

$$T_s = T_\infty + q''(R''_{t,conv}) = 20°\mathrm{C} + 100\ \mathrm{W/m^2} \times 0.1\ \mathrm{m^2 \cdot K/W} = 30°\mathrm{C}$$

$$T_C(x = L_A + L_B) = T_s + q''(R''_{t,cond,C}) = 30°\mathrm{C} + 100\ \mathrm{W/m^2} \times 0.04\ \mathrm{m^2 \cdot K/W} = 34°\mathrm{C}$$

$$T_B(x = L_A + L_B) = T_C(x = L_A + L_B) + q''(R''_{t,c}) = 34°\mathrm{C} + 100\ \mathrm{W/m^2} \times 0.01\ \frac{\mathrm{m^2 \cdot K}}{\mathrm{W}} = 35°\mathrm{C}$$

$$T_B(x = L_A) = T_B(x = L_A + L_B) + q''(R''_{t,cond,B}) = 35°\mathrm{C} + 100\ \mathrm{W/m^2} \times 0.1\ \mathrm{m^2 \cdot K/W} = 45°\mathrm{C}$$

and from part (a), $T_A(x = L_A) = 46°\mathrm{C}$. The temperature distribution is sketched below.

(c) For case 2, the heat flux in the range $0 \le x \le L_A + L_B$ is zero. Hence the boundary at $x = L_A + L_B$ acts as an insulated surface for material C. Therefore, from Eq. 3.43,

$$T_{max} = T_c(x = L_A + L_B) = T_s + \frac{\dot{q} L_C^2}{2k_C} = 30°\mathrm{C} + \frac{5000\ \mathrm{W/m^3} \times (0.02\mathrm{m})^2}{2 \times 0.50\ \mathrm{W/m \cdot K}} = 32°\mathrm{C}$$

The temperature distribution is sketched below.

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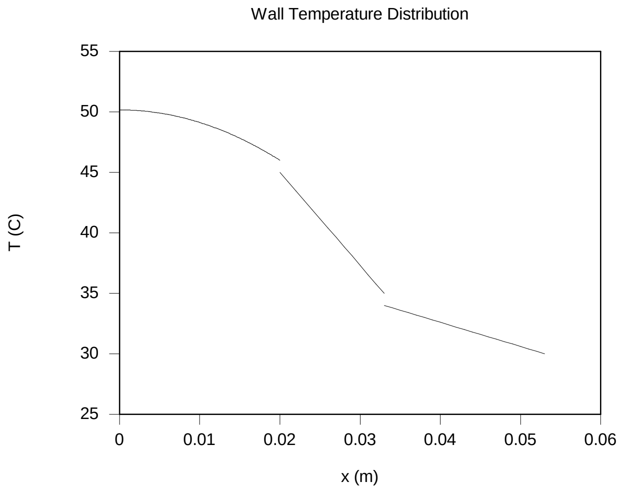
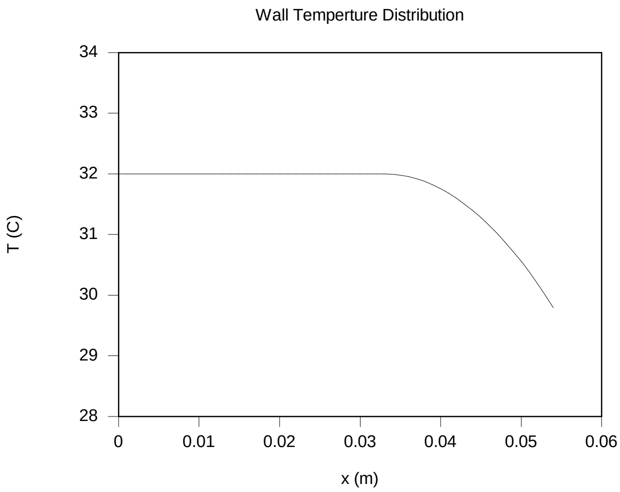
PROBLEM 3.85 (Cont.)



Case 1 temperature distribution.



Case 2 temperature distribution.

C**OMMENTS:** If the heat flux due to conduction in the x-direction is zero, the temperature gradient, dT/dx, must be zero. This is a direct consequence of Fourier's law, and holds under all conditions.